

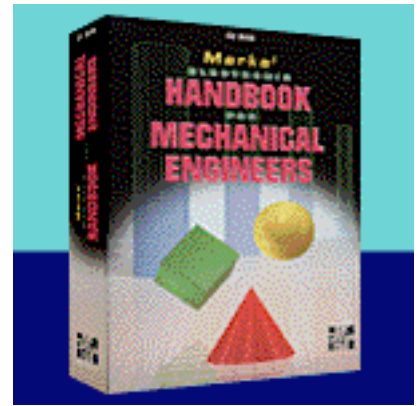
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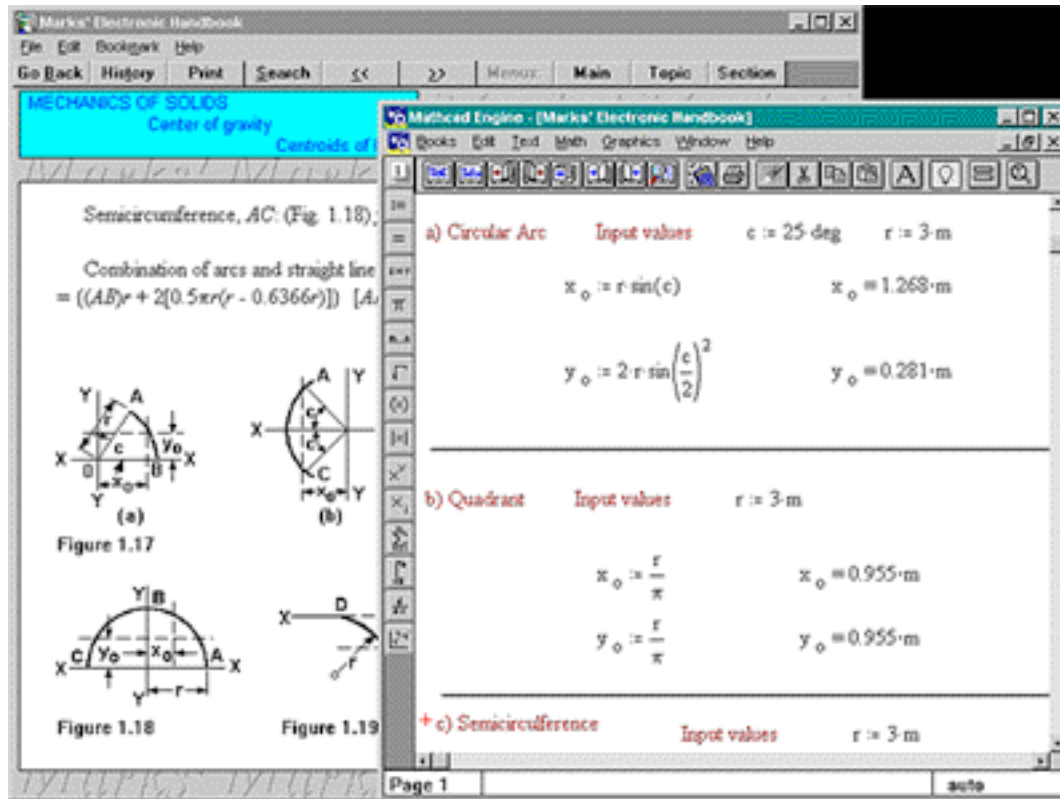


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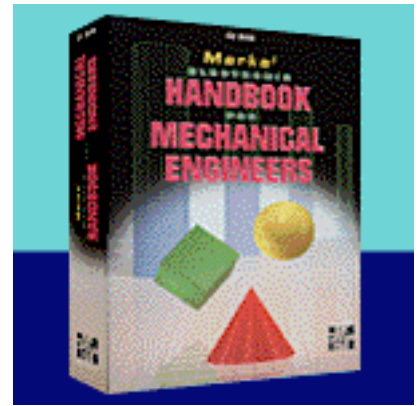


Explore the mechanics of solids by finding the center of gravity. All your calculations are 'live', so you can change a variable and watch Mathcad calculate the results automatically.

Topics include: Mechanics, Heat Strength of Materials, Gearing, Engines, Turbines, Pumps, Compressors, and more. Sections within each chapter cover Process and Operation, Principles and Theory, Formulas and Tables, Definitions, Tables, and more.

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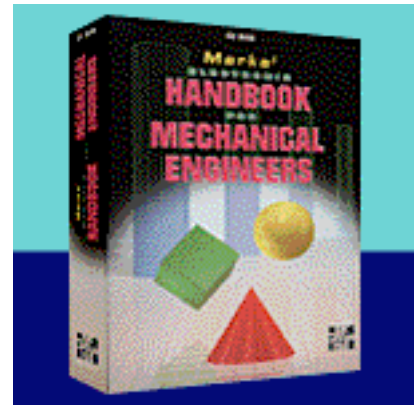


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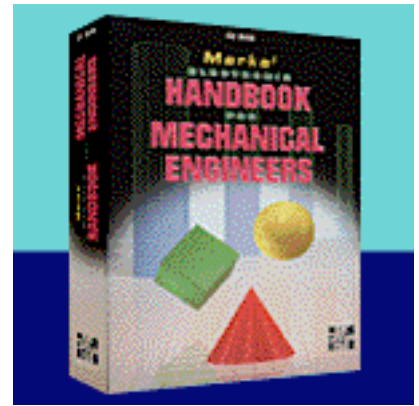
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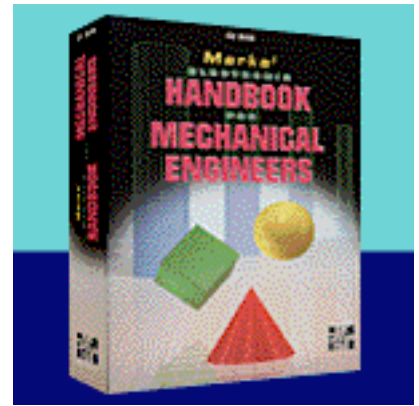
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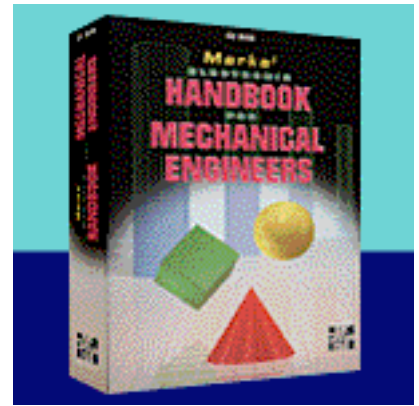
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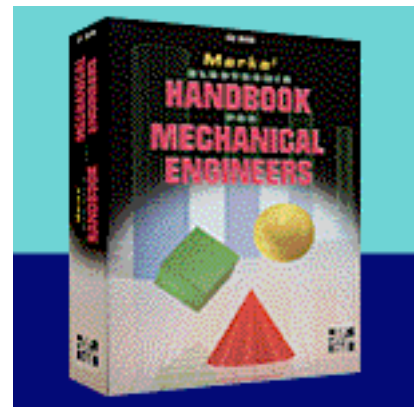
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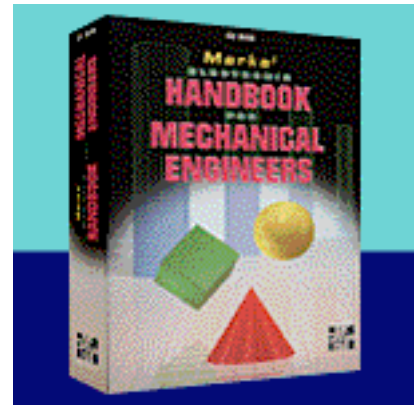


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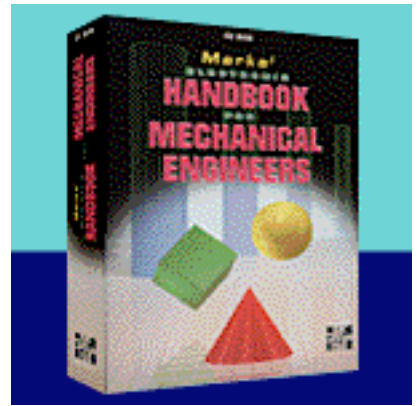
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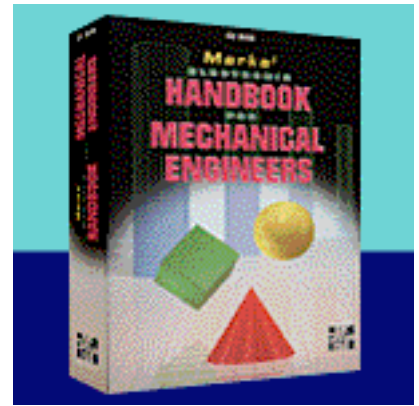
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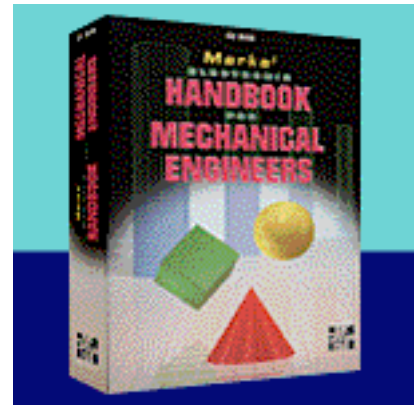
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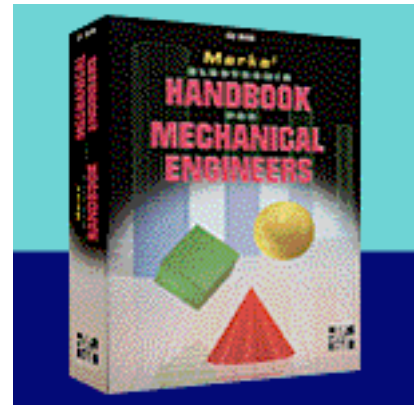
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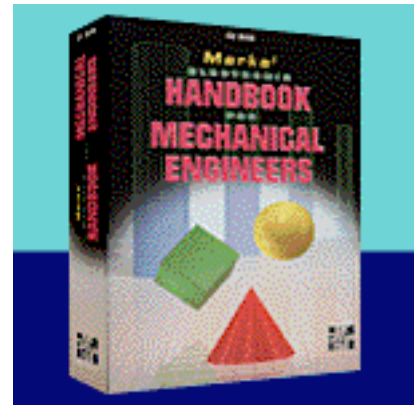
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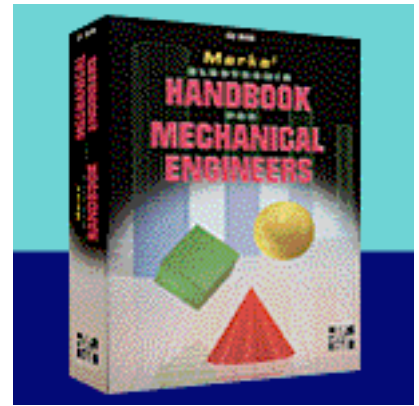
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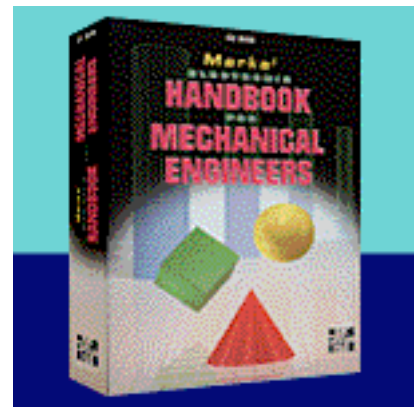
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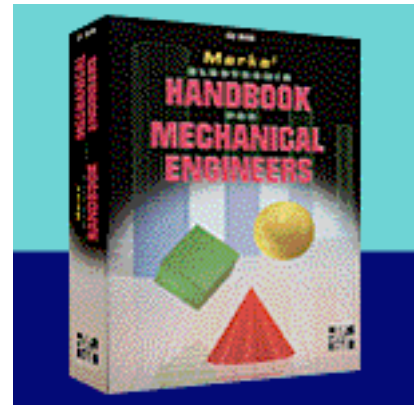


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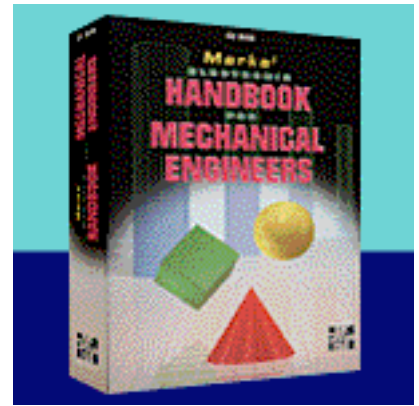
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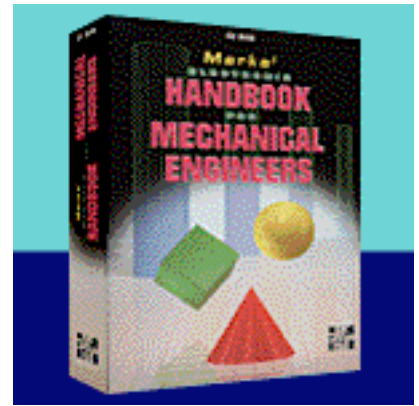
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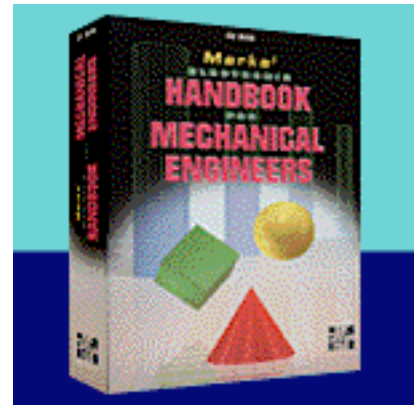
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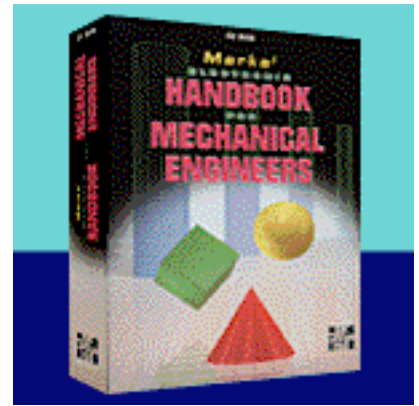
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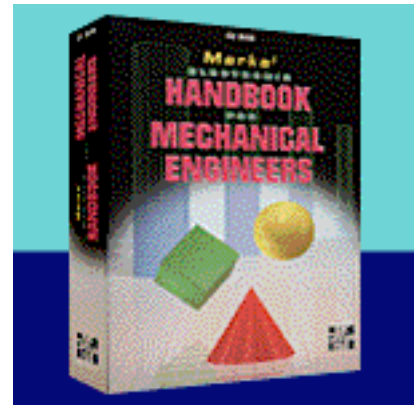
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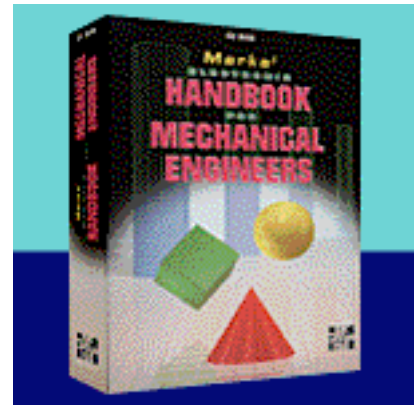
- Centrifugal pump variables
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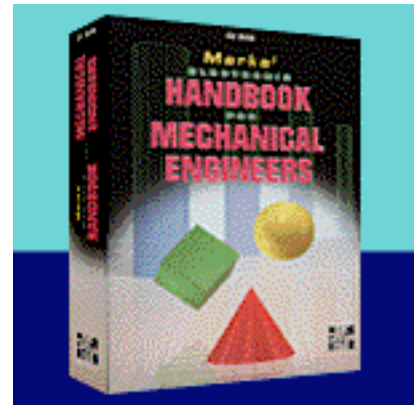
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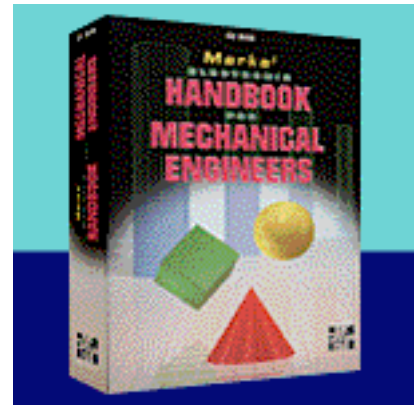
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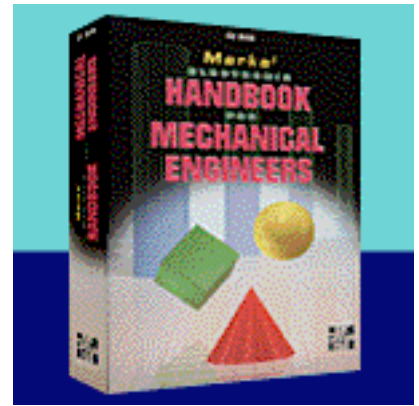
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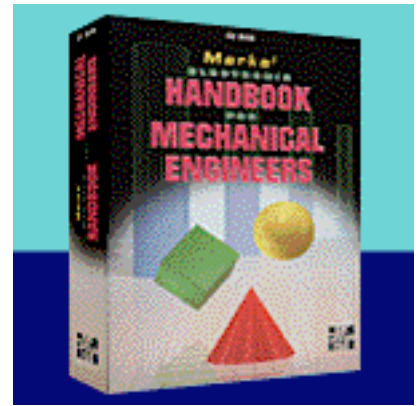


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HIGH-VACUUM PUMPS

Pipe flow of gases for high-vacuum systems

Knudsen number for high-vacuum systems

The conductance of a pipe depends on the geometry and the Knudsen number K (defined as the ratio of the mean free path of the gas molecules to the mean diameter of the cross section) as well as the direction and velocity of the molecules entering the pipe. For $K > 1$ the conductance for air in liters per second at 25°C of a circular pipe of length L (feet) and inside diameter D (inches) connecting a high-vacuum pump to a chamber of diameter greater than $3D$, including the "entrance correction" at the chamber, but neglecting the "exit correction" at the pump which depends on the inlet diameter and other factors, may be calculated from $U = 6.6D^3 / (L + 0.11D)$. The effect of right-angle bends in the pipe for "molecular flow" $K > 1$ and for $L > D/3$ may be approximated by adding $0.05D$ to L for each bend (where L is in feet and D in inches). A single right-angle bend in a short pipe ($L < D/3$) has practically no effect on the conductance as computed for a straight pipe of the same length along the centerline

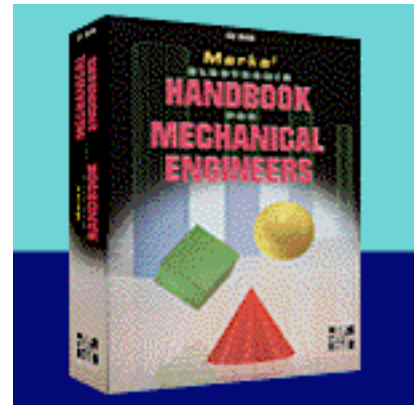
When $K < 0.01$, the conductance in liters per second for air at 20°C of a long circular pipe length L (feet) and diameter D (inches) may be calculated from $U = 0.25D^4P / L$, where P is the mean pressure in the pipe in millitorr (micrometers of Hg). For $0.01 < K < 1$ the conductance for air at 20°C of a long tube can be estimated from the following equation:

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(17.1)



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Input values

$$D := 50 \cdot \text{mm}$$

$$L := 2 \cdot \text{m}$$

$$P' := .0020 \cdot \text{torr}$$

$$U := \frac{0.25 \cdot D^4 \cdot P'}{L} + \left[\frac{1 + 0.65 \cdot D \cdot P' \cdot \frac{1}{\text{mm} \cdot \text{torr}}}{1 + 0.80 \cdot D \cdot P' \cdot \frac{1}{\text{mm} \cdot \text{torr}}} \cdot \text{mm} \cdot \text{torr} \right] \cdot \left(\frac{6.6 \cdot D^3}{L} \right) \quad U = 54.44 \cdot \frac{\text{kg} \cdot \text{mm}^2}{\text{sec}^2}$$

The size of the primary pump, which acts as a "roughing pump" to pump the chamber down from atmospheric pressure to a pressure at which a diffusion pump or other high-vacuum pump can operate, may depend on the peak gas load during the process as well as the desired pump-down time. However, the size indicated by the peak load condition is frequently much smaller than the size required to meet the specified pump-down or roughing time. In this case, if the process cycle is much longer than the pump-down time, it is advisable to use two forepumps (primary pumps), a large one for roughing down and a smaller one for holding the vapor pumps during the roughing period and backing them during the processing period. Roots-type blowers are useful for shortening the roughing time for large chambers in the range below 20 torr and for handling unusually large bursts of gas which occur in some processes.

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An oil-sealed rotary mechanical pump is normally used as the primary pump. The roughing time t_r (in minutes) required to evacuate a chamber of volume V (cubic feet) from atmospheric pressure to about 0.7 torr at which high-vacuum pumps begin to operate can be estimated from $t_r = 10VC$, where C is the rated speed (cubic feet per minute) at atmospheric pressure of the rotary pump. Since the speed of the high-vacuum pumps is usually of the order of 100 times that of the forepump, the pressure should drop quickly as soon as the high-vacuum pumps "take hold," but below 10^{-4} torr the pressure may begin to decrease more slowly because of the outgassing of the materials exposed inside the vacuum system.

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